

Delete, in its entirety, Table 13 on page 49 of the specification as filed and insert, in its place the following replacement Table 13 with the changes indicated at

Exhibit Tab A:

Table 13

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CONCENTRATION OF PEG (%)	pH	% POLYMER IN THE STARTING IVIG SOLUTION	CONCENTRATION OF SORBITOL (%)	PRESENCE OF PRECIPITATE (1)	(%) RECOVERY OF PROTEIN IN THE FILTRATE (2)
3.0	8.0	n.d.	0.4	YES (+++)	N.R.
3.0	8.0	n.d.	5	YES (+)	N.R.
3.0	8.0	n.d.	10	NO (-)	N.R.
3.0	8.0	3.97	9.4	YES (+++)	83.6
3.0	8.0	3.97	13.0	YES (+++)	92.2

IN THE CLAIMS:

Amend claims 20, 24, 42 and 44-46 as indicated on the attached Exhibit

A, so that the claims read as follows:

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20. (Once amended) A method for the production of virus-inactivated human gammaglobulin G according to claim 19 in which the filtered effluent is pasteurized in the presence of a sugar-alcohol.

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24. (Once amended) A method for the production of virus-inactivated human gammaglobulin G according to claim 23 in which, before said treatment with solvent/detergent, the pasteurised effluent is diluted with water for injection so that:

- (a) the concentration of sugar alcohol is 25% (w/w) or less, and
- (b) the concentration of protein is between 1% and 3% (w/v).

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42. (Once amended) A method for the production of virus-inactivated human gammaglobulin G according to claim 35, further comprising steps of:

- (a) adding an alkali to the acid solution so that the pH is adjusted to between 7.5 and 8.5, and
- (b) precipitating and separating insoluble high molecular weight aggregates from the pH adjusted solution.

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44. (Once amended) A method for the production of virus-inactivated human gammaglobulin G according to claim 42 further comprising, after separating insoluble high molecular weight aggregates from the pH adjusted solution, diafiltration and concentration of the solution, pH adjusted to 4.0 - 4.8, through ultrafiltration membranes of 100 kDa nominal molecular cut-off and at a transmembrane pressure below 1.2 bar.